

Math 332 Lecture 11

Conservation of mass, momentum, energy for a
constant density flow:

$$\text{mass: } \nabla \cdot \underline{u} = 0$$

$$\text{momentum: } \frac{\partial \underline{u}}{\partial t} + (\underline{u} \cdot \nabla) \underline{u} = -\frac{1}{\rho_0} \nabla \rho + \underline{g}$$

(per unit mass, per volume)

$$\text{energy: } \frac{\partial T}{\partial t} + (\underline{u} \cdot \nabla) T = \dots$$

For flow over a 2D airfoil, we replace
this system (coupled nonlinear PDEs) by

$$\nabla \cdot \underline{u} = 0$$

$$\nabla \times \underline{u} = 0$$

$$p + \frac{1}{2} \rho_0 \underline{u} \cdot \underline{u} = p_0 \text{ constant } \left[\frac{\text{force}}{\text{area}} \right]$$

$\nabla \times \underline{u} = 0$: the flow is "irrotational"

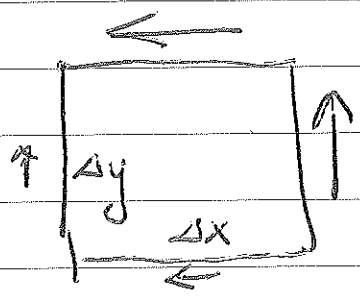
What does this mean?

Think about a 2D parcel of fluid

$$\underline{u} = \underline{u}(x, y) = u(x, y)\hat{x} + v(x, y)\hat{y}$$

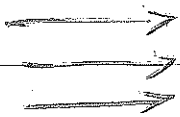
In Cartesian: $\nabla \times \underline{u} = \hat{z} \left(\frac{dv}{dx} - \frac{du}{dy} \right)$

IF $v(x)$ increases with x ; $u(y)$ increases with y



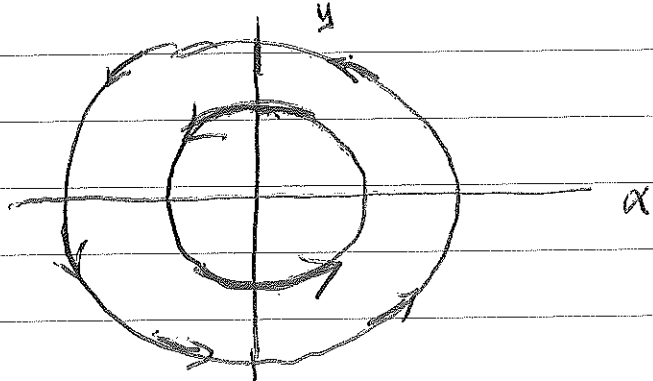
$\nabla \times \underline{u}$ is associated with local spin

Examples of irrotational flows:

① $\underline{u} = u_0 \hat{x}$  uniform flow

② $\underline{u} = u_r \hat{r} + u_\theta \hat{\theta} = (u_r, u_\theta)$

$u_\theta = \frac{k}{r}$, $u_r = 0$ $r > 0$



parcels not rotating locally as they rotate

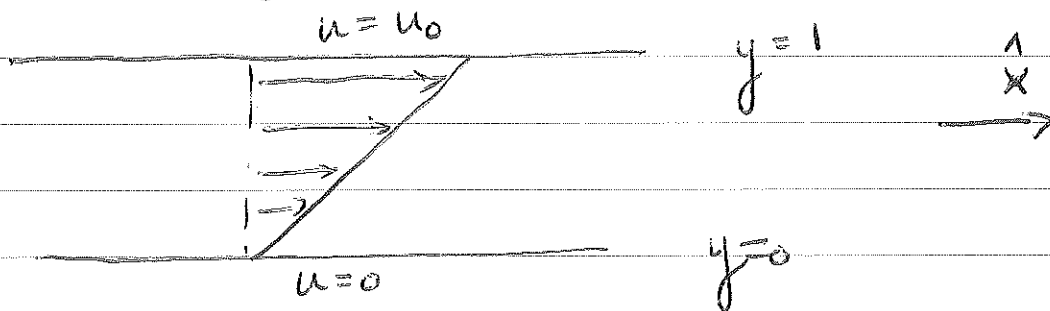
$$\underline{u} = u_r \hat{r} + u_\theta \hat{\theta} + u_z \hat{z} :$$

$$\begin{aligned} \nabla \times \underline{u} &= \frac{1}{r} \left(\frac{\partial u_z}{\partial \theta} - \frac{\partial u_\theta}{\partial z} \right) \hat{r} + \left(\frac{\partial u_r}{\partial z} - \frac{\partial u_z}{\partial r} \right) \hat{\theta} \\ &+ \frac{1}{r} \left(\frac{\partial}{\partial r} (r u_\theta) - \frac{\partial u_r}{\partial \theta} \right) \hat{z} \\ &= 0 \hat{r} + 0 \hat{\theta} + 0 \hat{z} \end{aligned}$$

What is NOT irrotational?

(i) Simple shear $\underline{u} = u \hat{x} + v \hat{y} = u_0 y \hat{x}$

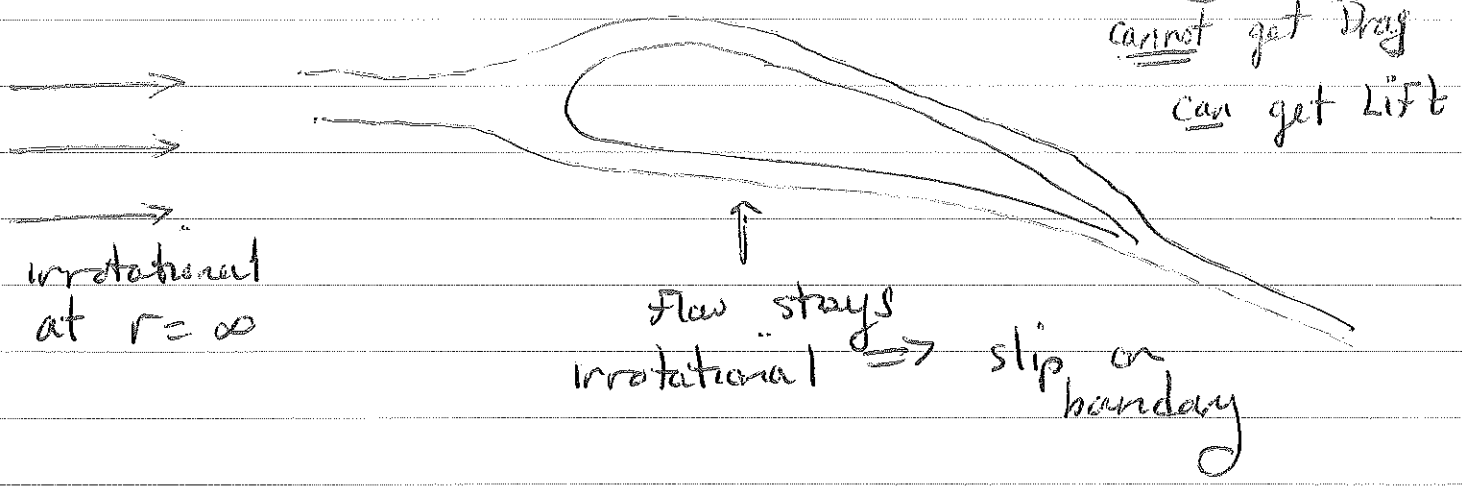
$$\nabla \times \underline{u} = - \frac{du}{dy} = -u_0$$



Since a fluid at the boundary will have the same velocity as the boundary \Rightarrow

boundaries (viscosity) create vorticity!

Ignore viscosity for flow over an airfoil;
all fluid to "slip" on the boundary



2D irrotational flow in Cartesian

* mass $\nabla \cdot \underline{u} = 0 \Rightarrow$

$$\underline{u} = \frac{\partial \psi}{\partial y} \hat{x} - \frac{\partial \psi}{\partial x} \hat{y} = (u, v)$$

$$\nabla \cdot \underline{u} = \frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = \frac{\partial}{\partial x} \left(\frac{\partial \psi}{\partial y} \right) - \frac{\partial}{\partial y} \left(\frac{\partial \psi}{\partial x} \right) = 0$$

* Then $\nabla \times \underline{u} = 0$

$$\frac{\partial v}{\partial x} - \frac{\partial u}{\partial y} = 0 = \frac{\partial}{\partial x} \left(-\frac{\partial \psi}{\partial x} \right) - \frac{\partial}{\partial y} \left(\frac{\partial \psi}{\partial y} \right) = -\nabla^2 \psi = 0$$

in Polar Coordinates $\underline{u} = u_r \hat{r} + u_\theta \hat{\theta}$

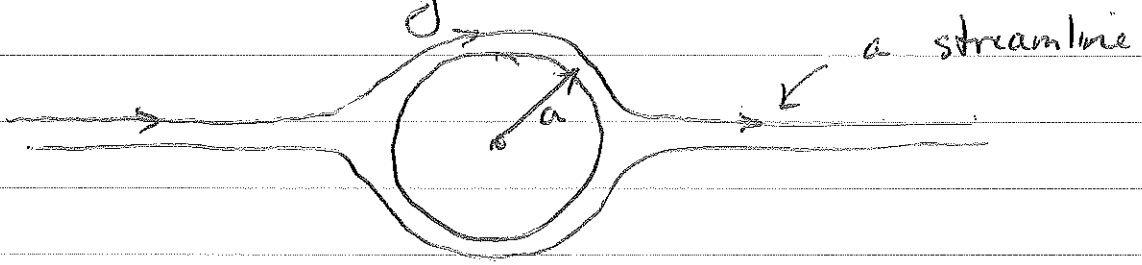
$$u_r = \frac{1}{r} \frac{\partial \psi}{\partial \theta}, \quad u_\theta = -\frac{\partial \psi}{\partial r} \quad \Rightarrow \quad \nabla^2 \psi(r, \theta) = 0$$

Check: $\nabla \cdot \underline{u} = \frac{1}{r} \frac{\partial}{\partial r} (r u_r) + \frac{1}{r} \frac{\partial u_\theta}{\partial \theta}$

$$= \frac{1}{r} \frac{\partial}{\partial r} \left(r \frac{1}{r} \frac{\partial \psi}{\partial \theta} \right) + \frac{1}{r} \frac{\partial}{\partial \theta} \left(-\frac{\partial \psi}{\partial r} \right)$$

$$= \frac{1}{r} \frac{\partial^2 \psi}{\partial r \partial \theta} + -\frac{1}{r} \frac{\partial^2 \psi}{\partial \theta \partial r} = 0 \dots$$

A streamline $\psi(r, \theta) = \text{constant}$ is everywhere tangent to the velocity vector



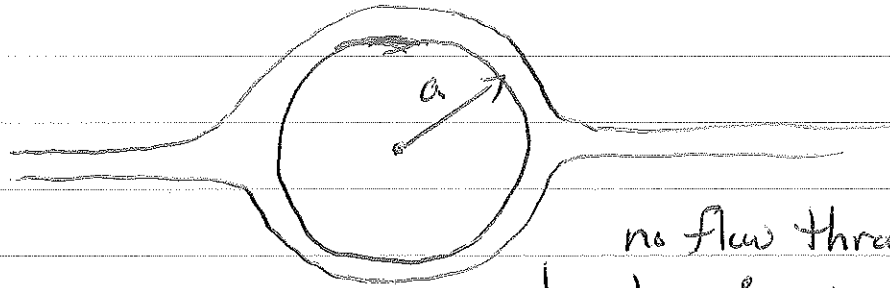
We've already solved $\nabla^2 \psi = 0$ with $\psi(a, \theta) = F(\theta)$ but now we are outside the circle

$$\psi(r, \theta) = A_0 + B_0 \ln r$$

$$+ \sum_{n=1}^{\infty} (a_n \cos n\theta + b_n \sin n\theta) (C_1 r^n + C_2 r^{-n})$$

What should we take for $F(\theta)$?
What other conditions do we need

Uniform
Flow in \hat{x}



no flow through the boundary: $u_r(a, \theta) = 0$

① Uniform Flow in \hat{x} : $\psi = U_0 y = U_0 r \sin \theta$

$\Rightarrow \lim_{r \rightarrow \infty} \psi(r, \theta) = U_0 r \sin \theta$

suggests keep only $n=1$, and the $\sin \theta$ term for $r \rightarrow \infty$

$\psi(r, \theta) = A_0 + B_0 \ln r + U_0 r \sin \theta + A_1 r^{-1} \cos \theta + B_1 r^{-1} \sin \theta$

check: $\lim_{r \rightarrow \infty} \psi(r, \theta) \sim U_0 r \sin \theta$

because the constant term and $\ln r$ terms are subdominant as $r \rightarrow \infty$

[$\ln(r)$ increases less rapidly than r as $r \rightarrow \infty$] ok

(2) Now apply no flow through boundary

$$u_r|_{r=a} = \frac{1}{r} \frac{\partial \psi}{\partial \theta} \Big|_{r=a} = 0 \quad \left[\frac{\partial \psi}{\partial \theta} \Big|_{r=a} = 0 \right]$$

$$\frac{\partial \psi}{\partial \theta} \Big|_{r=a} = (u_0 r + B_1 r^{-1}) \cos \theta \Big|_{r=a} - A_1 r^{-1} \sin \theta \Big|_{r=a} = 0$$

$$(u_0 a + B_1/a) \cos \theta - A_1/a \sin \theta = 0$$

$$\Rightarrow u_0 a + B_1/a = 0 \quad A_1 = 0 \quad \text{since}$$

$\sin \theta, \cos \theta$ are linearly independent

$$\Rightarrow \psi(r, \theta) = A_0 + B_0 \ln r + u_0 \left(r - \frac{a^2}{r} \right) \sin \theta$$

(3) Now what $F(\theta)$ do we take?

$$\text{Recall } \psi(a, \theta) = F(\theta)$$

$$\psi(a, \theta) = A_0 + B_0 \ln a + 0 = \text{constant!}$$

So the condition at $r = \infty$ and the no flow through body

force $F(\theta)$ constant, but

what constant?

Notice that there is an arbitrary constant in ψ that is not physical because ψ is an integral of the (physical) velocity field

$$\left\{ \text{Recall } u_r = \frac{1}{r} \frac{\partial \psi}{\partial \theta}, \quad u_\theta = -\frac{\partial \psi}{\partial r} \right\}$$

integrate to find ψ

\Rightarrow we can specify whatever we want for the constant value of $\psi(a, \theta)$

\Rightarrow choose zero for simplicity

$\Rightarrow \psi(a, \theta) = f(\theta) = \text{constant} = 0$
is a perfectly "good" choice, $\Rightarrow A_0 = -B_0/a$

Notice!

$$\lim_{r \rightarrow \infty} \psi(r, \theta) \sim u_0 r \sin \theta.$$

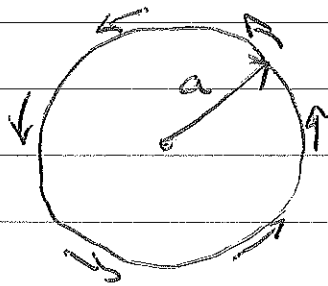
$\psi(a, \theta) = 0$ is not

enough for a unique solution because of the subdominant growth terms

$$[\ln(r)]$$

Finally $\psi(r, \theta) = B_0 \ln(r/a) + U_0 \left(r - \frac{a^2}{r} \right) \sin \theta$
 with 1 unknown coefficient B_0 .

Luckily we have one more physical consideration: the circulation around the airfoil is related to the "slip" velocity (tangential velocity) around the airfoil.



Circulation at $r=a$:

$$\int_0^{2\pi} u_{\theta}|_{r=a} a d\theta$$

Without viscosity, we have allowed any slip $u_{\theta}(a, \theta)$ and therefore any circulation

$$u_\theta = -\frac{\partial \psi}{\partial r} = - \left\{ B_0 \frac{1}{a} \frac{1}{r/a} + u_0 \sin \theta + u_0 \frac{a^2}{r^2} \sin \theta \right\}$$

$$u_\theta |_{r=a} = -\frac{B_0}{a} + 2u_0 \sin \theta$$

not determined because B_0 unknown

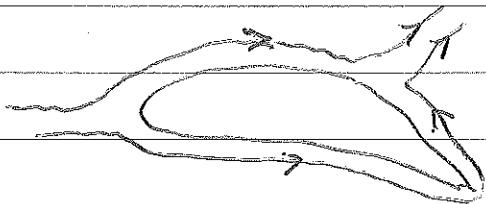
Circulation at $r=a$: $\int_0^{2\pi} u_\theta |_{r=a} a d\theta$

$$= \int_0^{2\pi} \left\{ -\frac{B_0}{a} + 2u_0 \sin \theta \right\} a d\theta = -2\pi B_0 = \Gamma$$

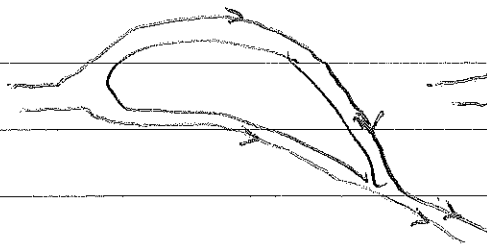
{ same for all closed contours in flow }

What value of circulation Γ should we choose?

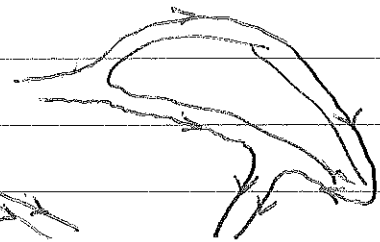
Now need to invoke viscosity!



No



Yes



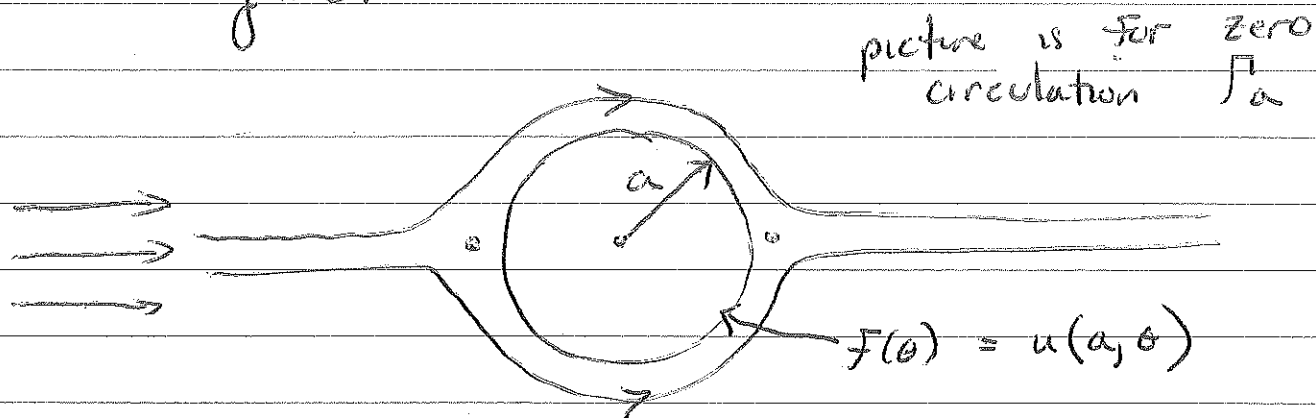
NO

viscosity doesn't like sharp gradients of velocity!

YES is a specific, negative value of circulation

Math 322 Lecture 12

Summary of the Flow over a circular cylinder



This is a special case of solving $\nabla^2 u = 0$
 with $u(a, \theta) = f(\theta)$; we want $u(r, \theta)$
outside

Here we call it $\nabla^2 \psi = 0$

The conditions ① Uniform flow at $r \rightarrow \infty$
 ② no flow through the body

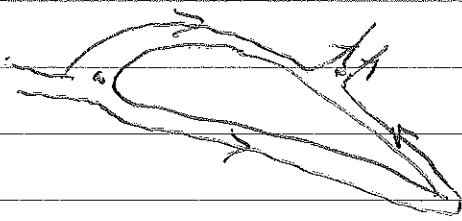
gives $f(\theta) = \text{constant}$ which we choose to
 be zero because ψ is an integral
 of physical velocity \Rightarrow the actual value
 of the constant has no physical meaning

We allowed any slip velocity (the picture
 above is only one special case; the
 physical case with stagnation points at

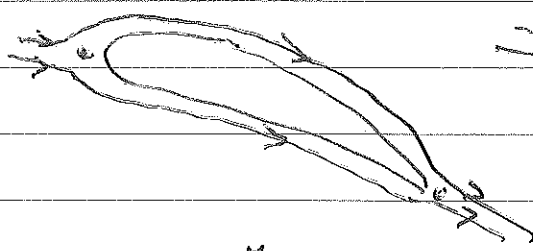
places that lead to zero circulation Γ_a)

$$\Gamma_a = -2\pi B_0 = \int_0^{2\pi} u_\theta|_{r=a} a d\theta$$

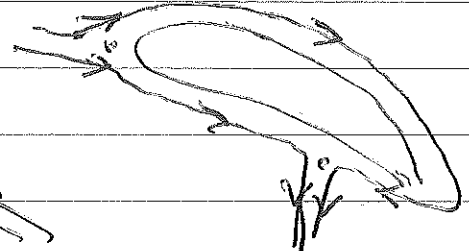
But the value of Γ_a we expect (physically) is negative



$\Gamma > 0$



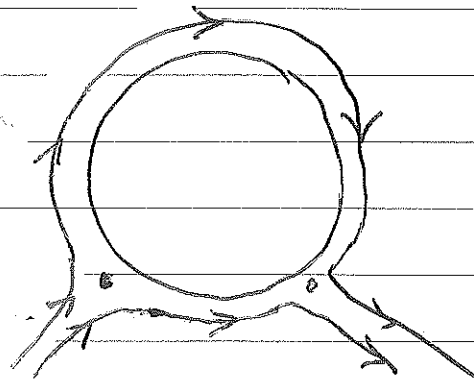
$\Gamma < 0$



$\Gamma < 0$

↓
viscosity chooses this circulation

corresponding to stagnation point at the sharp trailing edge, Kutta-Joukowski Condition



negative circulation

3

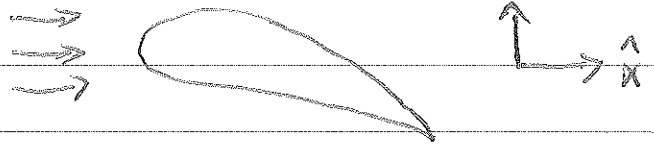
$$\psi(r, \theta) = B_0 \ln(r/a) + U_0 \left(r - \frac{a^2}{r} \right) \sin \theta$$

$$U_0 = -\frac{\partial \psi}{\partial r} \quad ; \quad u_\theta|_{r=a} = -\frac{B_0}{a} + 2U_0 \sin \theta$$

$$\Gamma_a = \int_0^{2\pi} u_\theta|_{r=a} a d\theta = -2\pi B_0 \quad \left(\begin{array}{l} \leftarrow 0 \text{ by} \\ \text{Kutta-Joukowski} \end{array} \right)$$

Lift and Drag

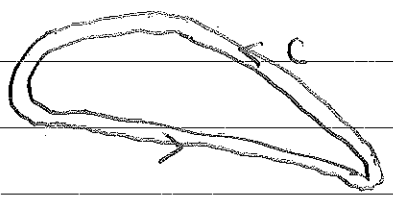
$$L = \underline{F} \cdot \hat{y} \quad D = \underline{F} \cdot \hat{x}$$



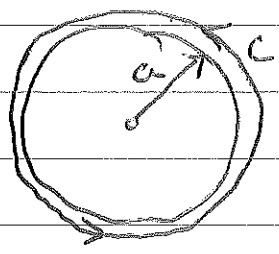
Normally both viscous and pressure forces, but here only pressure forces

Energy Eqn: $\rho + \frac{1}{2} \underline{u} \cdot \underline{u} = \text{constant} = p_0$

pressure is $\left[\frac{\text{Force}}{\text{area}} \right] \Rightarrow$ integrate over area to get Force



map



at $r=a$ fixed

$$L = \left(b \oint_c p_a (-\hat{n}) ds \right) \cdot \hat{y}$$

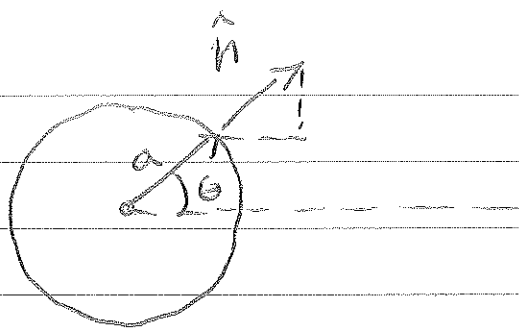
$b =$ width out of board

$$D = \left(b \oint_c p_a (-\hat{n}) ds \right) \cdot \hat{x}$$

{ 2D aero }

$p_a = \left(p_0 - \frac{1}{2} u_0 u_0 \right)_{r=a}$ no flow through cylinder

$$u_0 = - \frac{d\psi}{dr}$$



$$-\hat{n} \cdot \hat{y} = -\sin\theta$$

$$-\hat{n} \cdot \hat{x} = -\cos\theta$$

$$L = b \int_0^{2\pi} \rho_a (-\sin\theta) a d\theta = -\rho \mu_0 \Gamma b$$

where $\Gamma = -2\pi B_0$ negative

$$D = b \int_0^{2\pi} \rho_a (-\cos\theta) a d\theta = 0$$

"D'Alembert's paradox"

Do these calculations yourself! Homework 002